

# 1 **Property mapping of LDPE during 3D printing: Evaluating** 2 **morphological development with X-ray Scattering**

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12 **LDPE, polymer morphology, crystallization, SAXS/WAXS.**

## 13 **Abstract**

14 As part of the industry 4.0 implemented solutions, direct digital manufacturing has been ad-  
15 dressed as one of the key tools and it enables creation of products directly through digital definition.  
16 Commonly known as additive manufacturing, it comprises a set of technologies that are expressively  
17 agile in small-scale productions and prototyping and, in comparison to conventional mass  
18 manufacturing processes, such as injection molding of plastics. It streamlines mass customization and  
19 allows the production of highly complex objects; promoting new shapes obtained by generative design,  
20 weight reduction, and the concept of virtual part stocks for maintenance and production inventory.

21 It has been broadly applied in several fields, from medical devices to the aerospace industry. A  
22 new era of design possibilities and accessibility was unveiled; however, most developments are  
23 focused, merely, on shape reproduction precision and the development of new feeding systems and  
24 materials. This work is focused on a shift in design for additive manufacturing, where the defined  
25 polymer properties, by means of the adjustment of the process conditions, constitute a decision-making  
26 variable. In order to evaluate the morphology of semicrystalline polymers during extrusion-based 3D  
27 printing, in-situ time-resolving small and wide-angle X-ray scattering measurements were performed  
28 at the ALBA synchrotron light source in Barcelona. The ultimate goal of this research is to develop a  
29 material property mapping methodology during semicrystalline polymer melt extrusion-based 3D  
30 printing. For this purpose, some printing trials were performed with low-density polyethylene, and it  
31 was possible to observe a correlation between the extrusion rate, writing speed, and the level of  
32 anisotropy induced by the manufacturing parameters.

## 33 **1 Introduction**

34 Direct Digital Manufacturing (DDM ) consists of a decentralized scheme of manufacturing  
35 where designers and individuals (as consumers and makers) conceptualize products and innovative  
36 solutions allowing them to obtain small batches and mass customization for end users, making use of  
37 additive manufacturing as a base of the spectrum of technical solutions in which is possible to obtain

38 final parts and prototypes directly from a computer-aided design (CAD) file within a digital network  
39 and, optionally, validated through computer-aided engineering (CAE) software (1–3).

40 In comparison to conventional manufacturing technologies, DDM has enabled a more agile  
41 exploration of complex designs, and prototyping has become much faster and less expensive.  
42 Moreover, it has been established in industrial and commercial low-volume productions, and for  
43 customized tools (e.g., jigs, fixtures) (2). It is assumed that scientists and engineers have another set of  
44 technical solutions when designing for manufacturing, especially while working on complex and  
45 optimized geometries, engineered with topology optimization, generative design, or, simply, different  
46 infill strategies.

47 The advantage of mass customization is also beneficial for biomedical applications, where  
48 doctors and engineers combine strategies to create custom-fitting products for patients, such as in  
49 regenerative medicine, cancer therapies, and drug delivery systems (4).

50 Additive manufacturing (AM) comprises a variety of materials and processes, with extrusion-  
51 based technologies (such as FDM/FFF - fused deposition modeling/ fused filament  
52 fabrication) being the most accessible and popular solutions. Usually fed with filaments containing  
53 thermoplastic polymers, FDM/FFF equipment heat the material above the melting point, extrude  
54 it, and deposit it layer by layer, in predetermined patterns onto a build platform and predecessor layers,  
55 in order to complete a certain geometry (5,6).

56 In the last few years, many advances in 3D printing have been achieved, such as: object shape  
57 reproduction with higher accuracy (geometric and dimensional); higher print speeds (7); feeding  
58 systems along with material selection; and component integration (8). The range of available materials  
59 has followed this trend, widening to respond to the functionality requirements of the manufactured  
60 parts, including fiber reinforcement (9).

61 Attention has been given to the process parameters, such as printing temperatures and  
62 velocities, in order to optimize polymer melt flow rate (10). Besides that, there is an awareness of the  
63 influence of the manufacturing variables on the mechanical properties of the printed parts, as with any  
64 polymer processing technology (6). In some cases, in situ X-ray scattering analysis was performed  
65 along the printed layers, comparing the crystallization at different heights of the deposited strands, but  
66 lacking the evaluation along the write (print) direction with the variation of the fundamental processing  
67 parameters (11,12). In a similar way, but with the combined assessment of the temperature profile of  
68 the print, this technique was also used to infer the influence of the temperature profile on the degree of  
69 crystallinity (13). However, there is not a focus on the material design itself, beyond the domain of  
70 geometry replication.

71 The aim of this work is to address this area, introducing a new stage of design for additive  
72 manufacturing (DfAM). Ideally, the material properties can be mapped on de-mand along an entire  
73 part, through the control of the process parameters.

74 The challenge consists of understanding the correlation between the control inputs and the  
75 physical properties of the parts. This is the focus of this work, in which fused granular fabrication was  
76 used to perform printing trials with distinct sets of parameters, while analyzing the morphology  
77 development of the polymer melt; and in line with the previously reported work (14,15).

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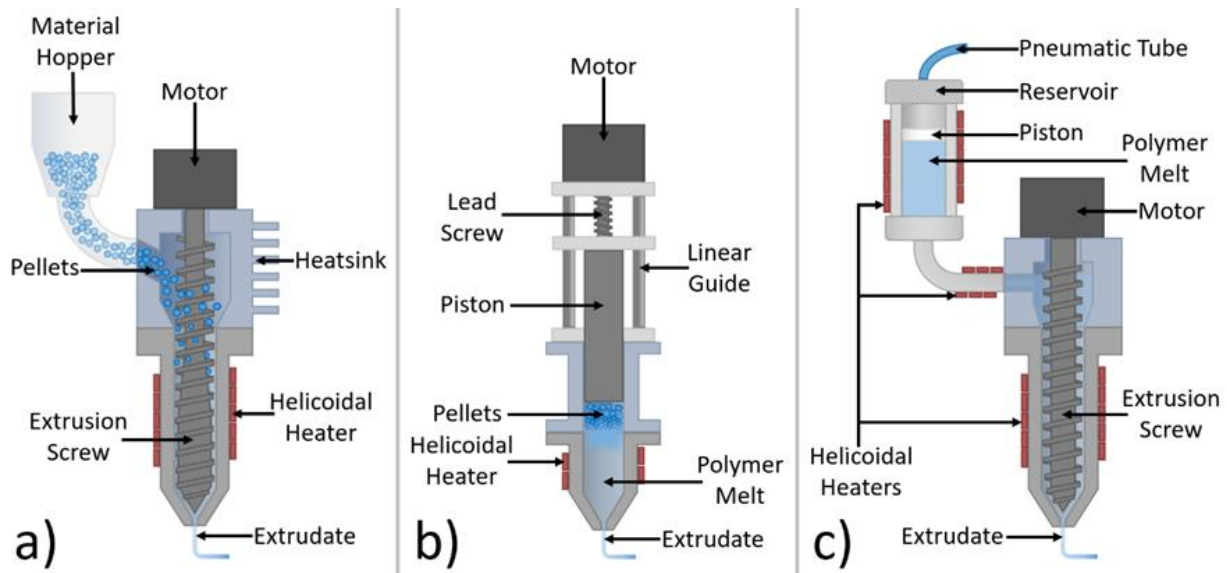
## 79 **1.1 Fused Granular Fabrication**

80 Fused granular fabrication (FGF) (or fused particle fabrication) (10) is an extrusion-based  
81 process that uses plastic pellets instead of a filament as the feedstock. In practice, it is a suitable  
82 approach for the production of bigger parts, and for the exploitation of the materials available on the  
83 market (typically deployed in injection molding) or custom compo-sites.

84 Usually, virgin material is obtained in pellet shape, and the same happens with recycled  
85 materials. Obtaining filament rolls implies an additional step, where the material is extruded with a  
86 certain diameter (usually 1.75mm or 3mm) and then wound. This filament production process might  
87 result in a slight degradation of the material, which can be considered a disadvantage of filament-fed  
88 3D printers (16,17). Besides, the use of pellets is very straightforward, and associated extrusion systems  
89 permit a relatively constant extrusion rate (with an even flow of homogeneous melt and without  
90 material feed blockages).

91 This work is based on a pellet-fed production, and, despite the availability of a large number of  
92 materials, and their grades, in this shape for injection molding, as an example; the successful  
93 implementation in 3D printing with melt deposition is deeply compromised by an elaborated set of  
94 distinct parameters and conditions, in comparison to conventional production technologies. In other  
95 words, the availability of a wider range of materials does not immediately mean that the pellet-shaped  
96 raw matter can be suitable for 3D printing. Instead, it means their potential applicability can be studied  
97 and explored. The FGF 3D printers share the same platforms FDM™/FFF printers, the only difference  
98 re-lies on the feeding/extruder system. Instead of a filament intake mechanism for the material to be  
99 pushed through a hot end, the extruder has a pellet hopper or a melt reservoir, to store and furtherly  
100 introduce the material in a solid or liquid state respectively, in the extruder barrel with a rotating  
101 extrusion screw (18–20). An alternative approach consists of filling a chamber with granules and  
102 utilizing a piston to press the heated material (21). The representation of these configurations can be  
103 observed in Figure 1.

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105

106 **Figure 1** - Representation of the types of fused granular fabrication extruders. a) extruder chamber directly fed with  
107 pellets; b) pellets placed and melt in the piston/plunger chamber; c) pellets placed and melt in the reservoir.

108 Basically, material feeding can occur in two ways: directly loading the extruder with pellets or  
109 loading it with the polymer melt.

110 In configuration a), from the reservoir, the beads enter the extrusion chamber (by gravity, or  
111 compressed air, and the motion of the screw itself), which has to be cooled to allow the transportation,  
112 at the feed zone, of the plastic material to the heated part where it is compressed and melt.

113 Configuration b) requires a full retraction of the piston to allow the refill of the chamber, the  
114 pellets are then compressed and melted in the same extruder part.

115 With configuration c), the material is placed and heated in a separate reservoir. The transport  
116 of the polymer melt is done by means of the movement of a piston, loaded with compressed air. Notice

117 that this configuration has three main heating zones: feeder, channel, and extruder body. Therefore,  
118 despite guaranteeing a uniform flow rate of material, this adds variables to control, to a list of  
119 parameters commonly involved in this form of additive manufacturing.

- 120
- 121 • Feeding system
  - 122 ○ Gravity
  - 123 ○ Size of the beads
  - 124 ○ Air pressure
  - 125 ○ Chamber heating
  - 126 ○ Polymer rheology
- 127 • Extruder temperature
  - 128 ○ Heating power
  - 129 ○ Insulation
  - 130 ○ Thermal conductivity and Heat dissipation of the extruder's body
  - 131 ○ Cooling system
- 132 • Extrusion rate/speed
  - 133 ○ Feeding system
  - 134 ○ Power input and mechanical transmission
  - 135 ○ Compression ratio
- 136 • Write/Print speed
  - 137 ○ Power input and mechanical transmission
  - 138 ○ Vibrations and damping
  - 139 ○ Mechanical elements and movement precision
  - 140 ○ Write/print and extrusion speed function (22)
  - 141 ○ Adhesion to bed/platform or to the previously deposited layers of material
- 142 • Printing platform/bed
  - 143 ○ Levelling
  - 144 ○ Platform material and finishing (for adhesion and/or heat conduction)
  - 145 ○ Bed temperature
- 146 • Nozzle/hot end configuration
  - 147 ○ Diameter
  - 148 ○ Length
    - 149 ■ Length-to-diameter ratio
  - 150 ○ Temperature
  - 151 ○ Material of the nozzle body
  - 152 ○ Geometry of the nozzle body
- 153 • Material
  - 154 ○ Rheology
    - 155 ■ Viscosity and melt flow index (MFI)
    - 156 ■ Temperature
    - 157 ■ Pressure
  - 158 ○ Thermal conductivity of the extrudate
  - 159 ○ Temperature differential between the layers
- 160 • Cooling system
  - 161 ○ Extrusion temperature

- 162 ○ Thermal conductivity of the extrudate
- 163 ○ Temperature of bed/platform or previously deposited layers of material
- 164 ● Surrounding environment
  - 165 ○ Enclosure hermeticity
  - 166 ○ Ambient temperature (air and radiant temperatures in closed and open environments)
  - 167 ○ Heat and matter transfer (air draughts and convection influence)
  - 168 ○ Humidity

169  
170 Exploring materials limits in 3D printing requires a set of instruments in order to monitor,  
171 control, and contour the above-listed variables (the levels of the list express the dependencies of each  
172 main parameter).

173 The time response of the input parameters differs between them, and for an “on de-mand” and  
174 “on the fly” control, it is rather convenient to have a practically instantaneous transition of the real  
175 value to the successive setpoints. Beyond that, the property mapping depends on the time it takes for  
176 the parameter shifts to have an effect on the material morphology, and the amount of time for relaxation  
177 and/or crystallization. The importance of these factors lies in the resultant precision and resolution of  
178 the induced property texture into the object’s material.

179 In practice, when set and read from the g-code file, a shift in extrusion rate or print speed  
180 happens substantially quicker than with the extrusion temperature. Not only this last variable has a  
181 noticeable delay associated, but it also has a more unstable behavior with successive heating and  
182 cooling switches around the target value, within a certain interval (overshooting and undershooting).

183 Although an effective extrusion temperature control could be employed, this paper focuses on  
184 the changes in the writing and extrusion speeds. Still, there are limitations such as the overall maximum  
185 velocity of the process, related to the mechanical transmission, and the movement precision or induced  
186 vibration.

187 The variety of materials previously referred to for FGF is available in the industry, directly  
188 obtained from chemical synthesis (virgin plastics of several grades) and recycling plants. In fact, the  
189 usage of recycled polymers in 3D printing has been investigated in order to reduce the environmental  
190 impact associated with “post-petroleum plastic sources” (16). Following this trend, this type of  
191 manufacture constitutes a possible promotor of the circular economy. This becomes effective by  
192 reintegrating the most widely used polymers in the first phases of the plastic value chain described by  
193 (23).

## 194 **1.2 LDPE in 3D Printing**

195 One of the most ubiquitous plastics is low-density polyethylene (LDPE). This polyolefin is  
196 mainly present in packaging, pipes, and houseware items, and is part of the seven main groups of  
197 recycled plastics (16,24). The use of LDPE in direct digital manufacturing is still very limited and  
198 challenging due to issues such as poor adhesion and high shrinkage (25,26). In fact, the production of  
199 LDPE filaments has been studied, tuning the extrusion parameters in order to produce usable filaments  
200 (27).

201 Nonetheless, the low melting temperature (typically from 105°C to 110°C) and the availability  
202 of great quantities at a small cost, turn the possibility of exploring a vast source of recycled raw material  
203 into an opportunity, increasing the value of extrusion-based 3D printing and the material itself.

204 Currently, LDPE has been studied in AM as a matrix for composites with higher  
205 biodegradability or with reinforcement particles (25, 28) as a potential material for patch antenna  
206 substrates (29), and as an additive itself on a blend with high-density polyethylene (HDPE) to fit its  
207 properties to 3D printing (25,30). Clearly, there is a wide interest on the application of this material in

208 3D printing, especially in the context of the implementation of circular economies. It is possible to  
209 incorporate additives in low-density polyethylene in order to promote dimensional accuracy, improve  
210 mechanical behavior (26, 31), and allow new applications. The exploration of material reinforcement  
211 is very significant when including recycled LDPE in the value chain since it has the potential of diluting  
212 the effects of degradation (from contaminants and broken molecular chains) induced by the recycling  
213 procedures. These additives work as nucleation agents which promote faster nucleation and a higher  
214 level of crystallinity, typically resulting in a higher rigidity. In the case of the present work, our ultimate  
215 goal is to reinforce the material by mapping its own properties during 3D printing, as a consequence  
216 of actively changing the process parameters. This paper describes the first of many studies to achieve  
217 that objective.

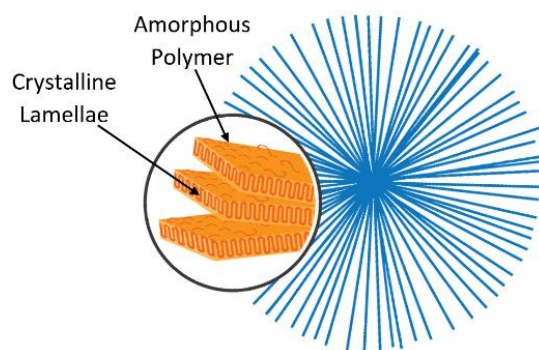
### 218 1.3 Melt flow conditions and morphology

219 The properties of objects manufactured from plastics do not entirely depend on the ingenuity  
220 of the molecule maker, as the structure and morphology which develop during the manufacturing  
221 process have a relevant role. In other words, the material properties are highly dependent on the process  
222 parameters. The most heavily used plastics in industry are semicrystalline (as it is possible to observe  
223 in (32)), in other words, they contain both amorphous and crystalline material. The majority of the  
224 matter is formed by the arrangement of single crystals, such as metals, in which the material consists  
225 of a large number of separate crystalline regions with grain boundaries between them. Large single  
226 crystals of polymers are not observed apart from the case of polydiacetylene which can be prepared  
227 from single crystals of the monomer via topochemical polymerization (33).

228 Crystallization processes, whether in a melt or in a solution, involve the processes of untangling  
229 the chains and then straightening them to add to the crystal growth face, although the precise details  
230 remain unclear. In 1957, a number of researchers deduced that the polymer chains folded at the top and  
231 bottom surfaces of the crystals which take the form of thin platelets about 10nm in thickness but up to  
232 several micrometers in the lateral directions (34).

233 Further work revealed that the chain folded lamellar crystals could develop in the framework  
234 of a spherulite in which crystals grew out from a common point in a crystallo-graphic direction lying  
235 in the plane of the lamellae (35).

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238 **Figure 2** - Schematic representation of a spherulite (semicrystalline structure).

239 Spherulites have been widely studied in polymer science, and the relationships of spherulite  
240 morphology to mechanical and other properties have been extensively explored. For instance, it was  
241 shown in early studies that the number and size of spherulites are directly correlated with the yield  
242 point and overall physical behavior of polymers (36,37).

243 Some efforts to better understand the local mechanical properties have been deployed for  
244 mapping along the spherulite radius (38), and to manipulate these structures during the process, with

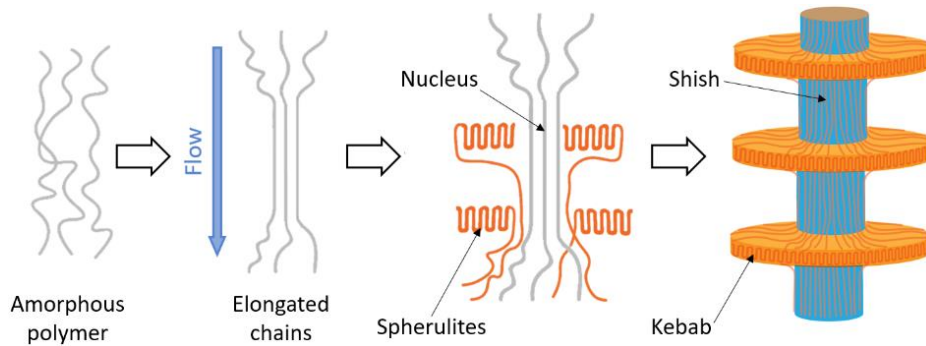


245 the application of new conditions such as nucleation agents and external loads, obtaining a better  
246 orientation of the lamellae and overall elongation (39).

247 Other arrangements are possible to observe when the lamellar crystals grow out from a common  
248 row nucleus, resulting in a higher level of anisotropy. Not surprisingly these different types of spatial  
249 arrangements exhibit different properties both with regard to mechanical behavior and degradation in  
250 the case of biodegradable polymers used in biomedical applications (40).

251 The formation of row nuclei can be associated with the development of extended chain  
252 conformations due to strain in a flow system (41). Equally highly anisotropic nanoparticles, such as  
253 carbon nanotubes (42) or self-assembling fibrillar nanoparticulate nucleating agents (43), can lead to  
254 higher anisotropic arrangements and a higher level of crystallinity. In the melt flow, this happens as a  
255 consequence of the common alignment of the nucleation sites, assuming that the common orientation  
256 of the particles introduced during the flow persists at the time crystallization is initiated.

257 The same mechanism can occur with the longest molecular chains in a polymer melt. this flow-  
258 induced orientation is often associated with the formation of shish-kebab semicrystalline structures  
259 (41,44) (represented in Figure 3).

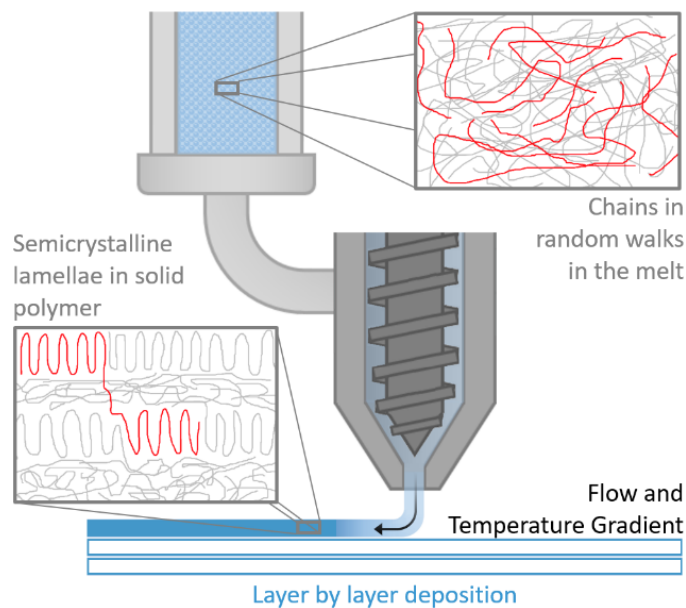


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261 **Figure 3** - Schematic representation of the formation of a shish kebab semicrystalline structure. Adapted from (45).

262 Basically, the longest chains (with higher molecular weight) become elongated due to the  
263 stresses in the flow. If, when reaching the crystallization temperature, these chains remain elongated,  
264 they template the nucleation (acting as row nuclei) for the surrounding polymer melt and chain folded  
265 lamellar crystals to grow out from. These lamellar crystals have their growth direction normal to the  
266 nuclei formed from the elongated chains (46).

267 In extrusion-based 3D printing, independently of the plastic part design, the polymer in the  
268 liquid phase is forced to pass through a restricting die (nozzle) with a certain length-to-diameter ratio  
269 (L/D). Even considering that the extrudate swells at the exit of the extruder (47), the resultant strand  
270 diameter is mainly defined by the nozzle diameter, and consequently, it defines the printing resolution,  
271 as observed in Figure 4.

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**Figure 4** - Representation of the polymer morphology overall change during FGF 3D printing. The two highlights, from left to right, respectively correspond to the melt in the reservoir and the deposited extrudate along the print.

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Shear stresses are applied in order to force the melt to pass through a constricted zone. For semicrystalline polymers (as it is illustrated in Figure 4), this condition induces the elongation of the larger chains (48), which can generate flow-induced oriented structures such as the shish-kebab arrangements presented in Figure 3. In practice, this results in a higher proportion of crystalline to amorphous material.

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These higher levels of preferred molecular alignment are expected to be translated into having a significant impact on the mechanical properties of the manufactured part. As an example, 3D printed objects can be mapped to be much stiffer in the longitudinal axis of the extruded strands, contrasting with a typical isotropic structure regularly obtained.

285

## 2 Materials and Methods

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### 2.1 Samples Material

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In this experiment, the samples correspond to the in-situ produced extrudates of semicrystalline thermoplastic. With the 3D printer analogous equipment, the trials were performed with low-density polyethylene (LDPE) from Repsol, the Alcludia® 1970C, with a melt flow index of 7.5 g/10min.

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### 2.2 X-ray Scattering Experimental Setup

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For the realization of the morphology analysis, the X-ray scattering was performed with synchrotron radiation, similarly to what has been performed by Mitchell, et al. (49); utilizing an especially developed apparatus, in this case, to replicate the extrusion-based 3D printer operation at the beamline. The facilities and the equipment are followingly de-scribed in the subsections 2.2.1 and 2.2.2.

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#### SAXS/WAXS Beamline

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Small-angle X-ray scattering (SAXS) and wide-angle X-ray scattering (WAXS) measurements were performed at the ALBA Synchrotron Light Source in Barcelona, using the NCD-SWEET Beamline (50). This beamline has equipment for the capture of SAXS and WAXS patterns



300 simultaneously. The SAXS patterns were obtained in a Q-range from 0.002 Å<sup>-1</sup> to 0.125 Å<sup>-1</sup> and the  
 301 WAXS patterns from 1.0 Å<sup>-1</sup> to 3 Å<sup>-1</sup>. The SAXS Detector is a Pilatus3S 1M system from DECTRIS,  
 302 a hybrid single photon counting system. The X-ray photon absorption in the detector leads to the  
 303 formation of electron-hole pairs and a charge proportional to the photon energy.

304 The Pilatus system is constituted by an arranged set of silicon sensors, and as a consequence,  
 305 approximately ~7% of the detector is intrinsically inactive (this unutilized zone appears as a black  
 306 stripes grid in the intensity recordings. Regarding the charge, it is detected and processed by the pixel  
 307 readout system, and the effective pixel has a dynamic range of 20 bits and a size of 172 x 172µm. In  
 308 order to prevent the saturation of the detector, a beam stop is placed in front of the detector to absorb  
 309 the zero-angle transmitted beam. The sample to SAXS detector distance was 6.73 m with an incident  
 310 X-ray wave-length of 1 Å. The detector orientation and sample-to-detector distance were calibrated  
 311 using the well-known standard silver behenate.

312 The WAXS detector was a Rayonix LX255 HS which is a triple cooled CCD detector bonded  
 313 to fiber optic tapers to the X-ray photon detector surface, with a pixel size of 44.27x44.27 µm. The  
 314 geometry of the detector ensures that the direct beam and the SAXS pattern are not blocked by itself.  
 315 The WAXS orientation and sample to detector distance were calibrated using Cr2O3. For each 2D  
 316 SAXS pattern an azimuthal section I(α) was obtained at constant |Q| and as a function of α, which is  
 317 the angle between the extrusion axis (vertical to the beamline) the beamline and the scattering vector  
 318 Q. The values of I(α) were necessary to evaluate the level of preferred orientation of the chain folded  
 319 lamellar crystals (given by <P<sub>2n</sub>><sub>Q</sub>), using the methodology developed by Mitchell (51–53),  
 320 represented in the equation below.

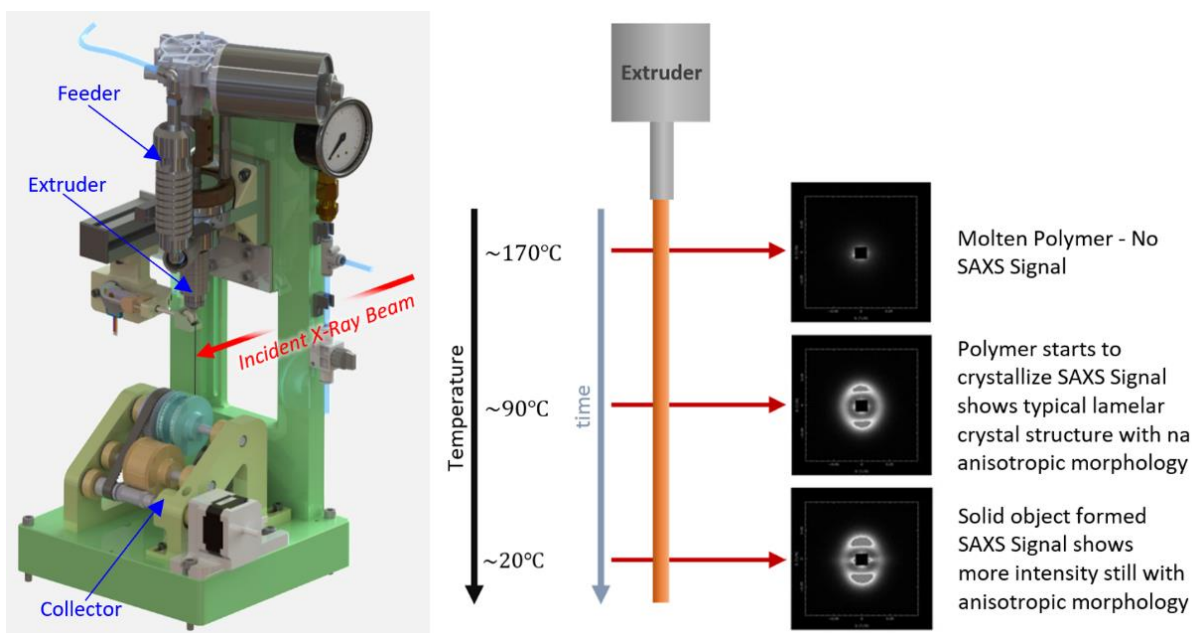
$$\langle P_{2n} \rangle_Q = \frac{1}{(4n + 1)P_2^m} \int_0^{\pi/2} \frac{I(|\underline{Q}|, \alpha) \sin \alpha P_2 (\cos \alpha) d\alpha}{I(|\underline{Q}|, \alpha) \sin \alpha d\alpha} \quad (\text{Equation 1})$$

321 This equation describes the orientation distribution function of the normal vectors to the  
 322 lamellar crystals (Q). The first component <P<sub>2n</sub>> is defined as the orientation parameter, and it reveals,  
 323 on a scale from 0 to 1 the level of anisotropy of the polymer morphology: if <P<sub>2n</sub>>=0, then the  
 324 morphology is isotropic; if <P<sub>2n</sub>>=1, then the crystals share the same alignment.

### 327 **Beamline 3D Printer**

328 One of the challenges of performing 3D printing trials at the ALBA synchrotron NCD-SWEET  
 329 beamline consisted of the process and equipment adaptation. For the experiment with low-density  
 330 polyethylene extrusion, the team of the present work resorted to the apparatus described in (14). It  
 331 consists of a device that can be mounted on the standard sample platform, and it was designed to allow  
 332 a continuous and stable extrusion, aligning the extrudate sample with the X-ray beam. The model of  
 333 the printer and the schematic of the experiment are presented in Figure 5.

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336 **Figure 5** – (Left) A CAD representation of the 3D printer developed for this work. (Right) A schematic of the quasi-static  
 337 state of the extrudate in a constant gradient of temperature (from the extrusion of the LDPE, passing through  
 338 crystallization, until cooling down to the surrounding temperature). The evolution of structure can be evaluated by  
 339 moving the incident X-ray beam down the jet. Adapted from (14).

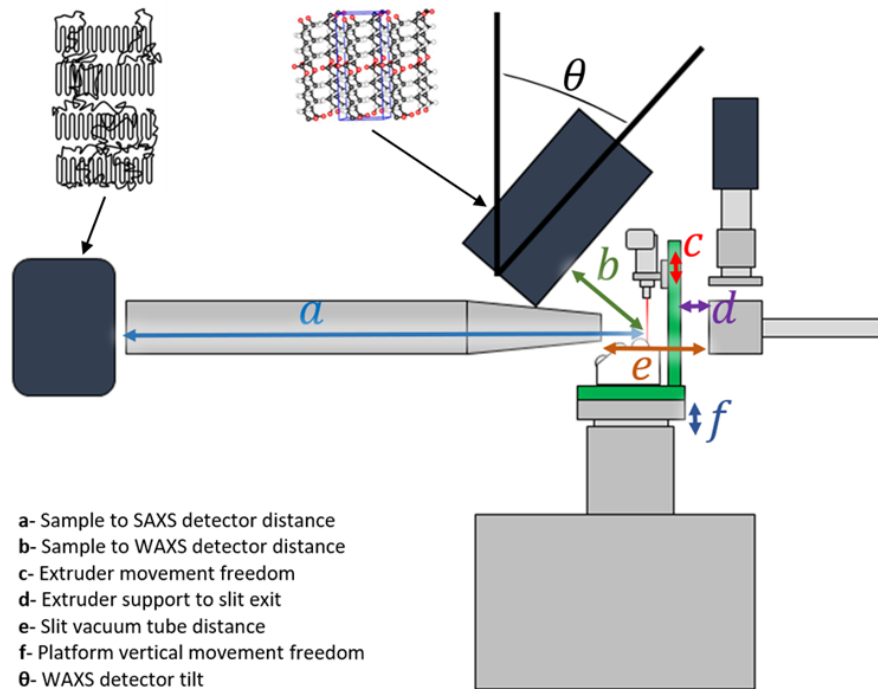
340 Comprising three main parts (feeder, extruder, and rotating collector), this equipment simulates  
 341 extrusion-based 3D printing along a moving platform, with a theoretically infinite path in a single  
 342 deposition direction (for a wider testing window).

343 This system is adjustable in the cartesian axis and uses a single extruder with a dual channel  
 344 screw to push the polymer melt through a needle with a high length-to-diameter ratio ( $L/D \approx 36$ ).

345 The FGF extruder utilized has a similar design to the one used in the bioextruder (20) (also  
 346 developed by a team of CDRSP- Polytechnic of Leiria), and it corresponds to the con-figuration c) in  
 347 Figure 1. Thus, it contains an attached material reservoir and three independent zones of temperature  
 348 control.

349 The communication with a microcontroller board enables the remote operation of the apparatus,  
 350 more specifically the control of the collector velocity (write/print speed), extruder screw rotation  
 351 velocity (extrusion rate), and the nozzle wiping mechanism.

352 Below, in Figure 6, a representation of the experimental assembly is presented, showing the 3D  
 353 printer mounted on the beamline platform, and the association of SAXS and WAXS detectors to the  
 354 scales of observation: lamellae morphology ( $\sim 100\text{\AA}$ ) and crystalline structures ( $\sim 10\text{\AA}$ ), respectively.  
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**Figure 6** - Representation of the 3D printer analogous equipment mounted on the NCD-SWEET beamline at the ALBA Synchrotron Light Source, with the domain of pattern observation of each detector. Adapted from (14).

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This representation shows the main dimensions related to the beamline facilities and the 3D printer. For the vertical adjustment of the area to be scanned, the distance between the needle outlet and the collector is variable by 50 mm.

The temperature profile of the extruded filament was maintained constant. Hence, it was possible to observe the extrudate in a quasi-steady state, in which the evolution of the structure and morphology with time could be assessed by moving up and down the platform; repositioning the incident X-ray beam along the extruded filament. Remotely and automatically controlled, a scan of 20 steps of 0.1mm with a 1-second data collection period could be retrieved, for each trial. A photograph of the equipment on the beamline is followingly presented in Figure 7.

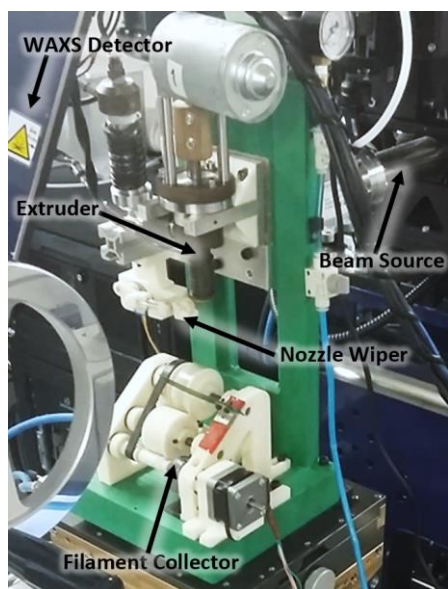


Figure 7 - Photograph of the equipment on the mounting stage of the beamline.

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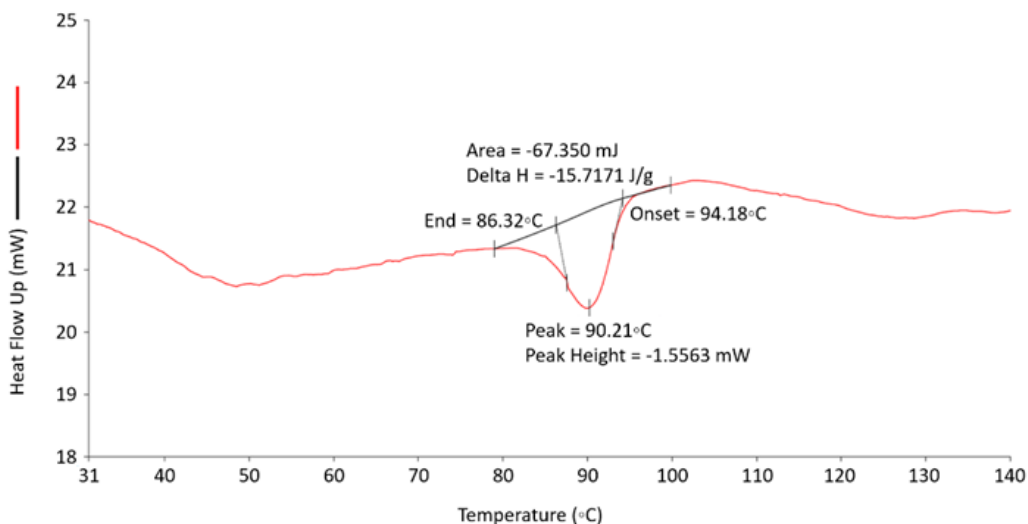
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### 372 3 Results and Discussion

#### 373 3.1 Crystallization Evaluation

374 The evaluation of the LDPE crystallization was performed using differential scanning  
 375 calorimetry (DSC) with a with a PerkinElmer STA 6000 thermal analyzer. Samples were heated from  
 376 30°C to 150°C at a rate of 10°C/min. A steady state at the maximum temperature was maintained for  
 377 5 minutes, followed by cooling back to 30°C at a rate of 5°C/min. The final cooling stage is represented  
 378 in Figure 8.



379

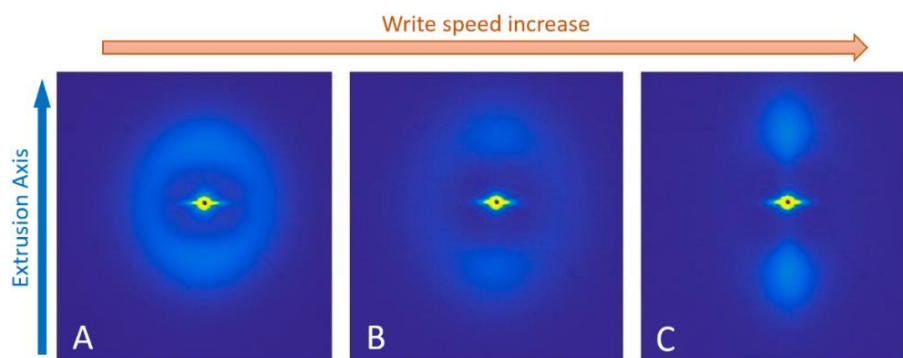
380 **Figure 8** - DSC cooling scan of a sample of LDPE used in this work from 150°C to room temperature (around 30°C)  
 381 showing the crystallization peak which reveals the maximum rate for a quiescent melt at 90.2°C.

382 In this domain of the DSC cooling scan, it is observed that in the quiescent material, the onset  
 383 of crystallization occurs at 94.2 °C while the maximum rate of crystallization is observed to be at a

384 temperature of 90.2°C. Notice that the material which has been extruded may start to crystallize at a  
385 higher temperature than the observed with the quiescent material, due to the presence of flow-induced  
386 row nuclei.

### 387 3.2 X-ray Scattering Analysis

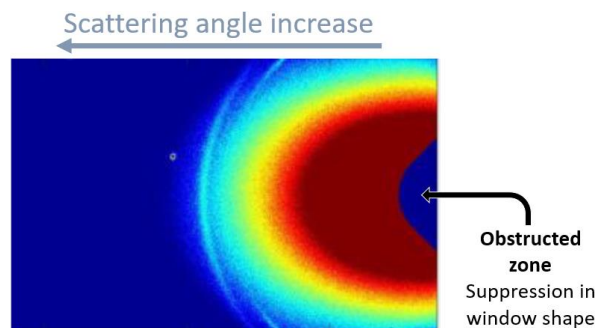
388 In this section, the results of the in-situ small and wide X-ray scattering analysis are presented.  
389 In Figure 9, the recorded SAXS scattering patterns of the filaments extruded with different write speeds  
390 (print speeds), maintaining the extrusion temperature and rate.  
391



392  
393 **Figure 9** - SAXS patterns from the last point of each scan down the extruded filament, at a temperature of 170°C, and a  
394 constant extrusion rate with different write/print speeds (increasing from A to C). Adapted from (15).

395 These SAXS patterns correspond to the point just before the build platform and are typical for  
396 a semicrystalline polymer. Pattern A shows a practically isotropic ring, indicating an isotropic  
397 distribution of the lamellar crystals. On the other hand, Figure 9C exhibits a highly anisotropic  
398 distribution of scattering suggesting a higher degree of order of lamellar crystals. The middle pattern  
399 (B) corresponds to an intermediate write speed, and it comprises both isotropic and highly anisotropic  
400 scatterings.

401 The WAXS pattern presented in Figure 10 was recorded in the same instant as the Figure 9C  
402 SAXS pattern. It shows the intense peaks for LDPE, the 110 and 200, corresponding to the arcs  
403 observed from right to left. Moreover, the development of an anisotropic morphology is indicated by  
404 the variation of the peaks' intensity in the azimuthal range.  
405

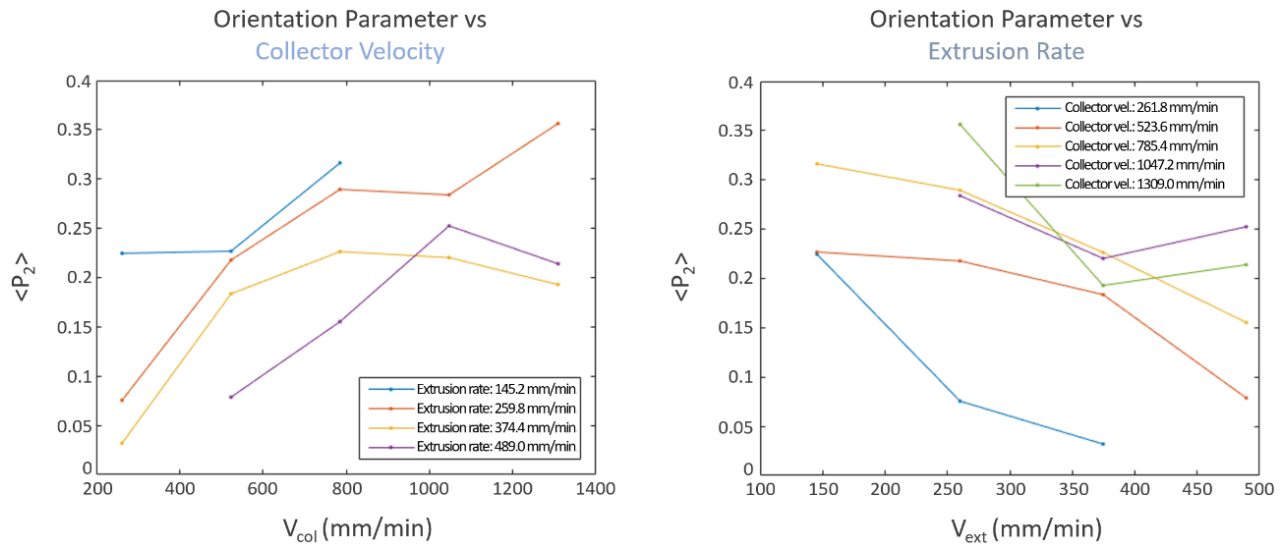


406  
407 **Figure 10** - WAXS pattern recorded at the same time as the SAXS pattern shown in Figure 9C. The scattering angle  
408 increases from left to right. Only the lower half of the angular range is shown in this figure, corresponding to a Q range of  
409 1 to 2 Å<sup>-1</sup>. Adapted from (15).

410 It is noticed that the anisotropy revealed in the WAXS pattern is less pronounced than the one  
411 observed with SAXS. This observation underlines the challenge of using wide-angle X-ray scattering  
412 to assess the orientation of structures in semicrystalline polymers. In the case of LDPE, the twisted

413 arrangement of chain-folded lamellar crystals is commonly observed. Thus, the preferred orientation  
414 of the lamellar crystals cannot be evaluated simply from WAXS patterns.

415 The preferred level of orientation of the lamellar crystals, the results are shown in Figure 11.  
416 The vertical axis corresponds to the orientation parameter  $\langle P_{2n} \rangle$ , obtained through Equation 1. Once  
417 again, this parameter can assume values from 0 to 1, respectively corresponding to a scale from  
418 completely isotropic to anisotropic morphology (uniform orientation of the crystalline structures).  
419



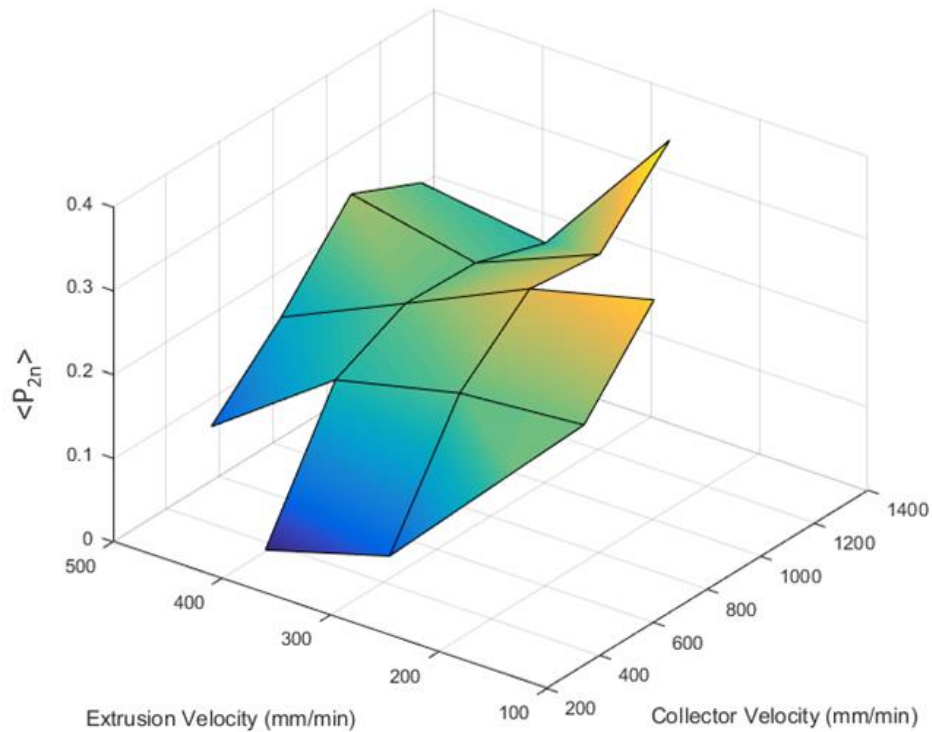
420  
421 **Figure 11** - Plots of the level of preferred orientation of the chain folded lamellar crystals in extruded strands of low-  
422 density polyethylene (LDPE) as a function of the collector velocity/print speed (on the left) and the extrusion velocity (on  
423 the right), at a constant extrusion temperature.

424 For the elaboration of both graphs, the temperatures of the 3 main zones of the extruder (feeder,  
425 channel, and extruder body) remained constant (extrusion temperature of 190°C). The left-hand plot  
426 corresponds to the variation of the preferred orientation level with the collector velocity (maintaining  
427 the extrusion rate value). The plot at the right corresponds to the variation of  $\langle P_{2n} \rangle$  with the extrusion  
428 rate (at constant values of collector velocity). Notice that printing speed is represented by the collector  
429 main roll rotation velocity given by the product of its angular velocity and radius.

430 In order to display any correlations between the preferred molecular orientation and extrusion  
431 and collector velocities, the three-dimensional plot shown Figure 12 was prepared, with the combined  
432 data from both plots in Figure 11.

433 Clearly, from the obtained results, it is possible to observe the final anisotropy level in LDPE,  
434 establishing a briefer correlation with both the extrusion and writing/print speeds (this one represented  
435 by the collector velocity), with the help of a color scale. The dark blue corresponds to the isotropic  
436 zone, and the yellow zones correspond to the higher anisotropy levels.  
437





**Figure 12** - Three-dimensional plot of the level of preferred orientation of the chain folded lamellar crystals in extruded strands of low-density polyethylene (LDPE) as a function of the extrusion velocity and the write speed (collector velocity) at a constant extrusion temperature, obtained from the conjunction of both graphs of Figure 11.

438

439

440

441

442 In summary, and in a broad observation, the level of preferred orientation of the chain folded  
 443 lamellar crystals is directly proportional to the collector velocity (write/print speed) and inversely  
 444 proportional to the extrusion rate.

445 In practice, during manufacturing, it represents that a more pronounced anisotropy value  
 446 (associated with higher elastic modulus) (14) is reached while extruding a smaller amount of material  
 447 along the same or a bigger path. This can be translated as a thinning of the deposited filament, and a  
 448 faster cooling rate.

449 Particular attention has to be given to the faster cooling rates and the thinning of the extrudate,  
 450 once it may compromise, in a counter-productive way, the interlayer adhesion, as well as the adhesion  
 451 between subsequently deposited filaments. Consequently, it may affect the mechanical properties and  
 452 behavior of the generated part (22).

453 This condition has to be considered in advance, during the part design. Usually, slicing software  
 454 provides these correlations in order to accomplish the intended geometries. However, if the design for  
 455 additive manufacturing strategy incorporates this thinning, another solution should be the revision of  
 456 the number of cycles/scans to fulfill a given length/width. Given the circumstances, it is not clearly  
 457 proven that faster deposition movements of the extrudate should consist of accelerated production.  
 458 Therefore, we can-not conclude, at some other level of process optimization, and with the actual data,  
 459 if the achievement of a higher level of anisotropy in semicrystalline polymers can be promptly or fully  
 460 associated with more agile production cycles. The use of higher extrusion speed doesn't necessarily  
 461 imply a higher manufacturing pace and may limit the overall rate of production.

462 Perhaps, new slicing strategies could be applied in order to optimize the anisotropy and,  
 463 consequently, obtain well-defined stiffer and softer zones, while maintaining a relatively normal to  
 464 fast-paced production.

465

## 466 **4 Conclusions and Future Work**

467 The main conclusion of the present work is that the adjustment of 3D printing parameters can  
468 be utilized strategically to affect the material morphology and structure along the fabrication of an  
469 object. Alternating the levels of preferred orientation of the lamellar crystals, it is possible to transcribe  
470 expected properties, correlated with the balance between isotropic and anisotropic distributions.

471 As an example, higher write speeds lead to faster cooling. For the same given temperature  
472 differential (from the nozzle to the cooled state of the deposited material), as the print speed increases,  
473 the extended chains, constrained and reoriented in the melt flow, don't have enough time to relax and  
474 remain mostly extended during crystallization, generating highly-aligned, therefore anisotropic  
475 morphology.

476 With a single material, the conception phase of a product can employ this morphology mapping  
477 strategy in order to set different mechanical properties. In the future, it should be expected the  
478 possibility to alter conditions and process parameters "on demand", during fabrication, to obtain  
479 desirable properties in particular zones of a single material manufactured part. This work is dedicated  
480 to promoting that approach, instead of considering, as in the current paradigm, that the pre-determined  
481 set of values should be maintained during the whole 3D printing production.

482 Certainly, and depending on the parameter to change (monitoring and control main variable),  
483 its set value is theoretically met within a certain period. How short or long that response turns out to  
484 be, in conjunction with the required time for those changes to have an effect on the material  
485 morphology, determines the resolution of the mapping.

486 Summarizing, controlling the core parameters of 3D printing induces changes in the material  
487 structure and morphology of semicrystalline polymers like LDPE. As a consequence, it is predicted  
488 that will affect the functionality of the printed part, allowing the enhancement of mechanical properties  
489 in a localized way. Therefore, more than reproducing a certain desired shape, it is believed that 3D  
490 printing may help develop new degrees of function for even more complex parts.

491 As this project is progressing, future works include studies about the rheological behavior,  
492 mechanical testing, 3D printing trials, the development of new products, and the influence of other  
493 variables such as the extrudate temperature.

494

## 495 **5 Conflict of Interest**

496 The funders had no role in the design of the study; in the collection, analyses, or interpretation  
497 of data; in the writing of the manuscript, or in the decision to publish the results.

498

## 499 **6 Author Contributions**

500 Conceptualization, GRM, DPS, JP; methodology, DPS. CKL, JCM, ES, GRM; software, GRM,  
501 JP.; validation, GRM, JP.; for-mal analysis, JP; investigation, JP, DPS, SA, PPF.; resources, X.X.; data  
502 curation, X.X.; writing—original draft preparation, DPS, GRM.; writing—DPS, JP, GRM PPF, X.X.;  
503 visualization, JP GRM.; supervision, GRM AM, PPF; project administration, GRM PPF; funding  
504 acquisition, GRM, PPF, AM. All authors have read and agreed to the published version of the  
505 manuscript.

506

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667

## 668 **10 Data Availability Statement**

669 The data obtained using the facilities of the ALBA Synchrotron Light Source are subject to the  
670 Generic data management policy at ALBA CELLS as can be accessed at [Microsoft Word -  
671 Data policy Alba v1.2 2017.doc \(cells.es\)](#). The experimental data identifiers are available from the  
672 corresponding author after the end of the embargo period.